

# Convection Heat Transfer of MgO-Ag /Water Magneto-Hybrid Nanoliquid Flow into a Special Porous Enclosure

Fateh Mebarek-Oudina<sup>1,\*</sup>, Fares Redouane<sup>2</sup> and Choudhari Rajashekhar<sup>3</sup>

<sup>1</sup>Department of Physics, Faculty of Sciences, University of 20 Août 1955-Skikda, Skikda, Algeria

<sup>2</sup>Department of Physics, LGIDD, University Center Ahmed Zabana, Relizane, Algeria

<sup>3</sup>Department of Mathematics, Vijayanagara Sri Krishnadevaraya University, Ballari, Karnataka, India.

\*Corresponding author; Email: oudina2003@yahoo.fr; f.mebarek\_oudina@univ-skikda.dz

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## ABSTRACT

This work explores numerically a computational study of free convection in a grooved porous enclosure filled with water-based hybrid-nanoliquid in the presence of an external magnetic field. To solve the governing equations of the problem, the Galerkin finite element technique is utilized. For a several governing parameters such as Rayleigh number ( $10^2 \leq Ra \leq 10^6$ ), magnetic field parameter ( $0 \leq Ha \leq 100$ ), Darcy number ( $10^{-2} \leq Da \leq 10^{-4}$ ) the results are obtained and discussed via streamlines, isotherms and average Nusselt number. The magnetic field has a good regulating effect for the fluid flow and the heat transfer in porous media.

## I. Introduction

The various applications of the free convection in industrial and engineering fields such as solar technology, heat exchangers, mobile device cooling, house heating and cooling systems, aeronautics, nuclear reactors, petrochemical industries and geophysical fluid dynamics are receiving significant attention from researchers and scientists around the world. The efficiency of thermal output depends on the creation of heat transfer mechanisms, especially as most engineering processes produce high temperatures. To do this, several approaches have been used to rise the efficiency of heat transfer in thermal engineering. Recently, referencing to Choi [1], nanoliquid, a colloidal blend of *NPs* into base liquids (such as water, ethylene glycol and oil), has been used to boost the effectiveness of heat transport mechanisms. As the rise in heat flow is an important problem for energy efficiency, free convection plays a crucial role in thermal engineering in nanoliquid inside enclosures. In this way, a variety of computational and experimental studies are performed. The research conducted by Khanafer et al. [2] listed as the initial efforts of heat transport improvement using nanoliquid. They simulated the problem of the nanofluid heat transfer characteristics in a two-dimensional enclosure, in their investigation the heat transfer rate increases significantly with the suspended nanoparticles at any value of Grashof. Mebarek-Oudina [3] inspected the thermal and hydrodynamic characteristics of Titania nanoparticles with different base fluids utilizing cylindrical annulus. Laterly Jou and Tzeng [4] applied a model to evaluate a related analysis in nanofluid-filled rectangular cavities. The heat transfer coefficient is important in nanofluids relative to pure fluids and grows with the rise of *Ra*. In a two-sided lid-driven square enclosure, Tiwari and Das [5] built a model to study the heat transport properties of nanofluids. The suspended nanoparticles improve the base liquid's heat transfer potential, which is more pronounced with an augment in the solid volume fraction. Also, the differing *Ri* numbers and the moving walls directions influenced fluid flow and heat transfer within the cavity. Various studies using different nanoparticles

and base fluids are published by different authors [6-31]. Kakac and Pramuanjaroenkij [32] found that nanofluids dramatically increase the ability of thermal processes to transfer heat. Izadi et al. [33] utilized the numerical method to analyze the effect of nanoparticles concentration and inclination angle of on mixed convection in an inclined square enclosure with a moving top wall. In another publication, Izadi et al. [34] analyzed the thermal non-equilibrium model with free convection inside a porous cavity in a micropolar nanofluid. The heat transfer rate in the porous medium rises with a reduce in the thermal resistance of the fuel domain with an augment in the thermal conductivity ratio. Sabour et al. [35] examined the free convection of nanofluid in a square enclosure. They revealed that the improvement in heat transfer is ensured as the volume of nanofluid increases with Rayleighs number. The efficiency of the employ of nanofluids influenced by the nanoparticles shape as well as the base liquid is also observed. In a nanofluid square cavity with separate inner geometries, Roy [36] conducted a computational analysis of free convection, the Nusselt number increases linearly with the rise in the nanoparticle volume fraction. He noticed that the form of various inner geometries influences the rising rate of the heat transfer coefficient. Bondarenko et al. [37] studied a free convection cooling device utilizing a heat-generating source and a heat-conducting portion at diverse positions on the bottom wall of a square enclosure. They found that the cooling efficiency depends on the position of the heat source due to the addition of nanoparticles in the base liquid. Using Buongiorno's nanofluid model, Elshehabey and Ahmed [38] analyzed the mixed convection in a lid-driven enclosure. Noghrehabadi et al. [39] investigated the free convection flow of nanofluid in a square cavity in the presence of heat source and sink. On the other hand, the study of electrically conducting fluid in the presence of magnetic field effect has significant applications in industrial and engineering fields such as crystal growth in liquids, cooling of microelectronic devices and nuclear reactors. Bourantas and Loukopoulos [40] utilized mesh less point collocation with velocity correction technique to simulate the transient free convection flow of micropolar nanofluid in an inclined square enclosure subjected to a magnetic field. The flow and temperature are affected significantly by the strength and orientation of magnetic field. Kasaeipoor et al. [41] studied the effect of magnetized Cooper-Water nanofluid mixed convection flow in a T-shaped cavity and proposed that some range of  $Re$  number and  $Ha$  number depends on rising heat transport rate with augmenting volume fraction. With magnetic field, Job and Gunakala [42] studied the impact of joule dissipation and viscous on two-dimensional unstable buoyancy-driven Alumina-water and SWCNT-water nanofluids in a wavy trapezoidal enclosure. They reported that the flow propagation diminishes and the rate of heat transfer rises for greater wavy bottom wall amplitude. As the intensity values and the inclination angle of the magnetic field increase, the rate of heat transfer decreases. The flow and thermal fields influenced by the variable thermal boundary conditions are also analyzed. In a differentially heated hexagonal enclosure, Ali et al. [43] introduced the finite element method to analyze MHD free convection flow. They studied the effect of the magnetic field on free nanofluid convection in a grooved cavity with varying thermal conditions. Due to the varying thermal conditions, flow and thermal fields are greatly affected. Also with the increase in the Rayleigh number and the nanoparticles volume fraction, the rate of heat transfer increases. An experimental investigation of the effect of the free convection in a differentially heated cubic enclosure is made by Dixit and Pattamatta [44]. They also shown that due of the magnetic field effects, the heat transport rate turns down. Alsoy-Akgün [45] later extended the Dual Reciprocity Boundary Element Approach (DRBEM) to model unstable free convection in Alumina-water nanofluid into square enclosure subjected to an uniform magnetic field. Due to  $Ra$  number, the effect of magnetic field on heat transfer efficiency and temperature profiles depends on buoyancy power. The effect of the concentration of nanoparticles on the liquid behaviors associated with the magnetic field parameter effect is also observed. Izadi et al. [46] are numerically studied the free convection in magnetized hybrid nanofluid-filled porous enclosure. With rising porosity coefficient and  $Ha$  number, the heat transfer rate increases and decreases. The fractional volume of nanoparticles affects the streamlines. Ideal geometric modifications with additional surfaces such as fins, grooves, corrugations and baffles can also increase the performance of thermal devices. Therefore, for a basic geometric model, the disadvantage of the lower heat transfer rate motivated us to create a new geometric model with square grooves to improve the heat transport rate. In this respect, numerous experiments with various configurations are carried out to study the activities of flow and heat transfer. Han and Rhi analyzed experimentally the thermal efficiency of a grooved heated pipe filled with nanofluid and hybrid nanofluid [47]. They found that thermal resistance is high with increasing concentrations of nanoparticles. With the presence of an adiabatic baffle, Sharma et al. [48] studied mixed convection in a grooved channel. They concluded that the rate of heat transfer rises due to the presence of a baffle in this mode of convection. Kumar et al. [49] published an experimental analysis on turbulent free convection in a cavity with a smooth or grooved bottom area in the presence of heat flux. A numerical study on the mixed convective flow of nanofluids in a grooved channel like solid cylinders with the effect of magnetic field is carried out by Job and Gunakala [50]. They showed that the diverse groove geometries, cylinder radius and other related parameters influenced flow and thermal fields.

It is clear from the analysis of the literature that there is no research on free convection in a special enclosure filled with MgO-Ag / water hybrid nanofluid (50%-50%). Additionally, it is possible to use the magnetic field to regulate fluid flow and heat transfer.

The object of this work is to analyze numerically the thermal and dynamic field of the flow in terms of streamlines, and isotherms in the presence of a magnetic field in a porous medium.

In the construction of thermal equipment such as heat exchangers, electronic cooling equipment and biomedical equipment where high temperatures and fluid flow need to be controlled, the forecasts and even the results of this type of study can be a useful reference.

## II. Problem Description

Figure 1 describes the physical model of the present investigation. The working fluid inside the enclosure is assumed as water. Ag, MgO are the nanoparticles used here [52], where  $T_c$  is the initial temperature.

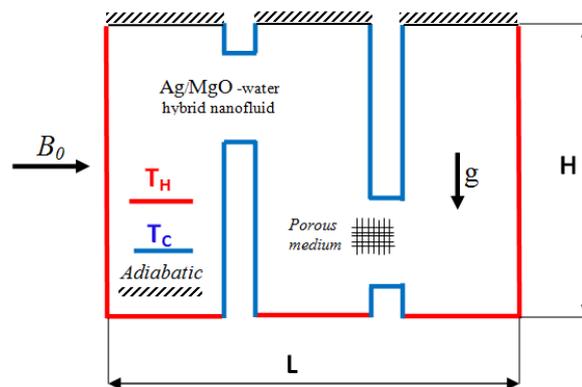


Figure 1. Scheme of the grooved enclosure used.

The thermo-physical properties of the base fluid and nanoparticles used here are detailed in Table 1.

Table 1. Base liquid and nanoparticles properties. [52]

	H <sub>2</sub> O	MgO	Ag
$C_p$ (J/kg·k)	4179	765	383
$\rho$ (kg/m <sup>3</sup> )	997.1	3600	8954
$K$ (W/m·k)	0.6	46	400
$\beta \cdot 10^{-5}$ (K <sup>-1</sup> )	21	0.63	1.67
$\sigma \cdot 10^{-6}$ ( $\Omega^{-1}m^{-1}$ )	5.5	2.7	59.6

## III. Validation and Grid Test Analysis

This numerical simulation is validated by comparing the present numerical results with the previously published results. We have used our numerical code to simulate the identical problem of those Ghasemi et al. [51]. The comparison shows that the results are consistent with each other. From the Fig. 2 the contours of total entropy generation are almost identical.

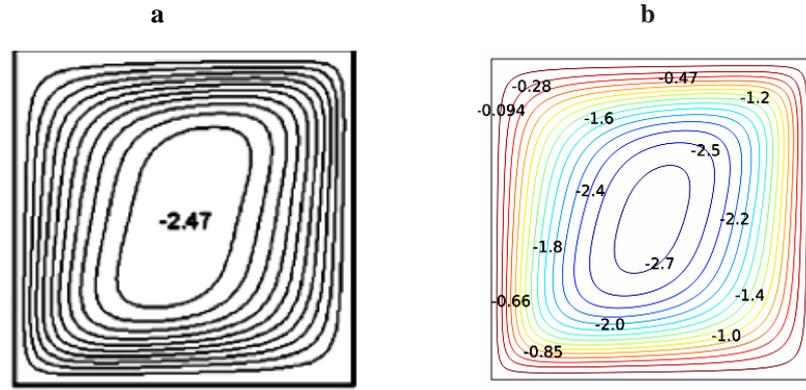


Figure 2. Streamlines results at  $Ra = 10^5$ , a)Ghasemi et al. [51], b)Present work.

Table 2. Grid dependency of  $\psi_{max}$  at the left heated wall when  $Ra = 10^6$ ,  $Ha = 0$ ,  $\phi = 0.05$  and  $Da = 0.1$ .

Number of elements	1898	4678	7258	17248	<b>42548</b>	53190
$\psi_{max}$	7.2665	7.2275	7.2143	7.1994	<b>7.1977</b>	7.1976

### IV. Development model

The dimensionless governing equations are:

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} = 0 \tag{1}$$

$$\frac{1}{\varepsilon^2} \frac{\rho_{hnf}}{\rho_{bf}} \left( U \frac{\partial U}{\partial X} + V \frac{\partial U}{\partial Y} \right) = -\frac{\partial P}{\partial X} + \frac{1}{\varepsilon} \frac{v_{hnf}}{v_{bf}} \frac{Pr}{\sqrt{Ra}} \left( \frac{\partial^2 U}{\partial X^2} + \frac{\partial^2 U}{\partial Y^2} \right) - \frac{v_{hnf}}{v_{bf}} \frac{Pr}{Da\sqrt{Ra}} U - \frac{F_c}{\sqrt{Da}} |u|U \tag{2}$$

$$\frac{1}{\varepsilon^2} \frac{\rho_{hnf}}{\rho_{bf}} \left( U \frac{\partial V}{\partial X} + V \frac{\partial V}{\partial Y} \right) = -\frac{\partial P}{\partial Y} + \frac{1}{\varepsilon} \frac{v_{hnf}}{v_{bf}} \frac{Pr}{\sqrt{Ra}} \left( \frac{\partial^2 V}{\partial X^2} + \frac{\partial^2 V}{\partial Y^2} \right) - \frac{v_{hnf}}{v_{bf}} \frac{Pr}{Da\sqrt{Ra}} V - \frac{F_c}{\sqrt{Da}} |u|V + Pr \frac{\beta_{hnf}}{\beta_f} g\theta + \frac{\sigma_{hnf}}{\rho_{hnf}} \frac{\rho_{bf}}{\rho_{hnf}} \frac{PrHa^2}{\varepsilon \sqrt{Ra}} V \tag{3}$$

Energy:

$$U \frac{\partial \theta}{\partial X} + V \frac{\partial \theta}{\partial Y} = \frac{\sigma_{hnf}}{\sigma_{bf}} \left( \frac{\partial^2 \theta}{\partial X^2} + \frac{\partial^2 \theta}{\partial Y^2} \right) \tag{4}$$

Where  $\alpha_{hnf} = \frac{(\rho c_p)_{bf} k_{hnf}}{(\rho c_p)_{hnf} k_f}$  is the thermal diffusivity of the nanofluid,  $|u| = \sqrt{u^2 + v^2}$  amplitude velocity

$F = \frac{b}{\sqrt{a}\varepsilon^{3/2}}$  denotes the Forchheimer coefficient (where  $a = 150$  and  $b = 1.75$ ).  $k_{eff}$  defines the operative thermal conductivity of porous medium saturated with nanofluid, where for the porous medium  $K$  is the permeability, and  $\varepsilon$  is the porosity of the medium, that can be described as:  $K = \frac{\varepsilon^2 d_m^2}{150(1-\varepsilon)^2}$ . The following dimensionless variables are employed to transform these governing equations:

$$X = \frac{x}{L}, Y = \frac{y}{L}, U = \frac{uL}{\alpha_{bf}}, V = \frac{vL}{\alpha_{bf}}, \theta = \frac{T-T_f}{T_h-T_f}, P = \frac{(p+\rho_{0bf}g_y)L^2}{\rho_{bf}\alpha_{bf}^2} \tag{5}$$

Dimensionless numbers are written as:

$$Pr = \frac{v_{bf}}{\alpha_{bf}}, Da = \frac{K}{L^2}, Ha = LB_0 \sqrt{\frac{\sigma_{bf}}{\mu_{bf}}}, Ra = \frac{\beta_{bf}g(T_h-T_f)L^3}{\alpha_{bf}v_{bf}} \tag{6}$$

The associated dimensionless boundary conditions are :

1. On the internal walls:

$$U = V = 0, \theta = 0 \tag{7}$$

2. On the top horizontal walls

$$U = V = 0, \frac{\partial \theta}{\partial Y} = 0 \quad (8)$$

3. On the bottom horizontal and vertical walls:

$$U = V = 0, \theta = 1 \quad (9)$$

#### IV.1. Nanofluid Thermophysical Characteristics

Designed for nanoparticles MgO and Ag, the properties are obtained :

$$\varphi = \varphi_{MgO} + \varphi_{Ag} \quad (10)$$

$$\rho_{np} = \frac{\varphi_{MgO} \rho_{MgO} + \varphi_{Ag} \rho_{Ag}}{\varphi} \quad (11)$$

$$(c_p)_{np} = \frac{\varphi_{MgO} (c_p)_{MgO} + \varphi_{Ag} (c_p)_{Ag}}{\varphi} \quad (12)$$

$$\beta_{np} = \frac{\varphi_{MgO} \beta_{MgO} + \varphi_{Ag} \beta_{Ag}}{\varphi} \quad (13)$$

$$k_{np} = \frac{\varphi_{MgO} k_{MgO} + \varphi_{Ag} k_{Ag}}{\varphi} \quad (14)$$

$$\sigma_{np} = \frac{\varphi_{MgO} \sigma_{MgO} + \varphi_{Ag} \sigma_{Ag}}{\varphi} \quad (15)$$

$$\sigma_{hnf} = (1-\varphi) \sigma_{bf} + \varphi \sigma_{np} \quad (16)$$

$$\rho_{hnf} = (1-\varphi) \rho_{bf} + \varphi \rho_{np} \quad (17)$$

$$(\rho\beta)_{hnf} = (1-\varphi) (\rho\beta)_{bf} + \varphi (\rho\beta)_{np} \quad (18)$$

$$(\rho c_p)_{hnf} = (1-\varphi) (\rho c_p)_{bf} + \varphi (\rho c_p)_{np} \quad (19)$$

$$\alpha_{hnf} = \frac{k_{hnf}}{(\rho c_p)_{hnf}} \quad (20)$$

$$\frac{k_{hnf}}{k_{bf}} = \frac{k_{np} + (n-1)k_{bf} - (n-1)(k_{bf} - k_{np})\varphi}{k_{np} + (n-1)k_{bf} + (k_{bf} - k_{np})\varphi} \quad (21)$$

The effective dynamic viscosity based on the Brinkman mode is considered as

$$\mu_{hnf} = \frac{\mu_{bf}}{(1-\varphi)^{2.5}} \quad (22)$$

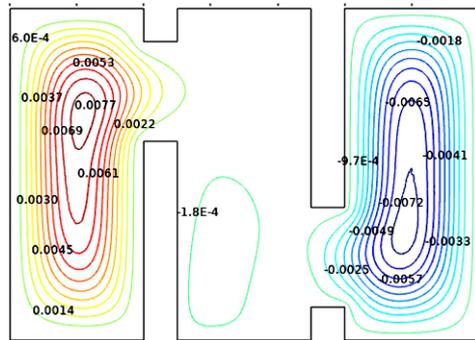
The electric conductivity and the thermal conductivity respectively:

$$\frac{\sigma_{hnf}}{\sigma_{bf}} = 1 + \frac{3(\sigma_{np} - \sigma_{bf})\varphi}{(\sigma_{np} + 2\sigma_{bf}) - (\sigma_{np} - \sigma_{bf})\varphi} \quad (23)$$

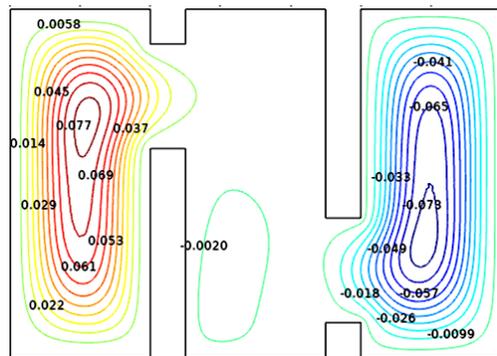
$$Nu_{local} = \frac{k_{hmf}}{k_{bf}} \frac{\partial T}{\partial y} \tag{24}$$

$$Nu_{average} = \frac{1}{L} \int_0^L Nu_{local} dL \tag{25}$$

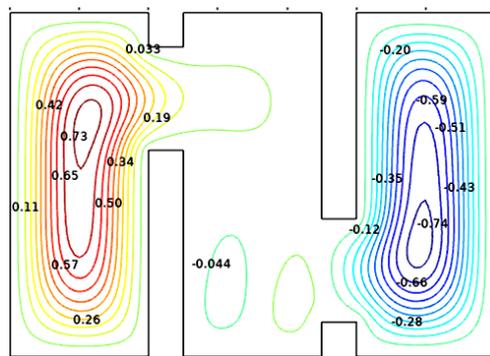
## V. Graphical illustration & Discussion



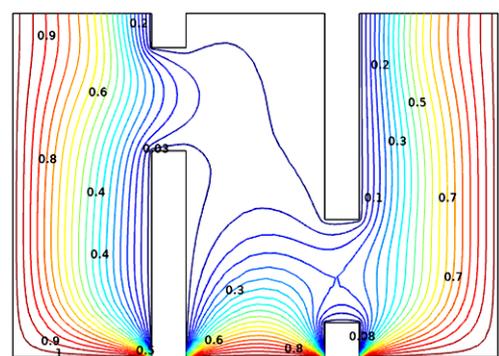
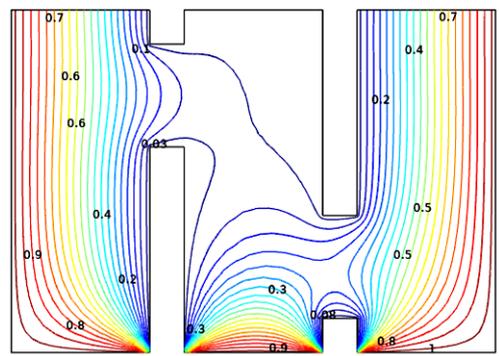
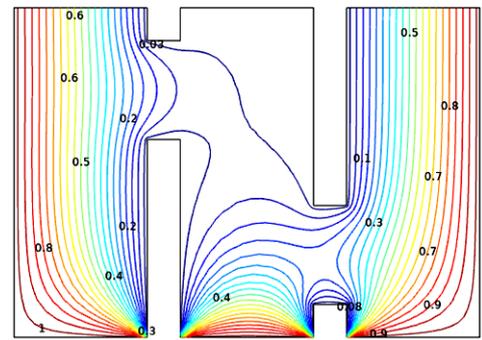
(a)  $Ra = 10^3$



(b)  $Ra = 10^4$



(c)  $Ra = 10^5$



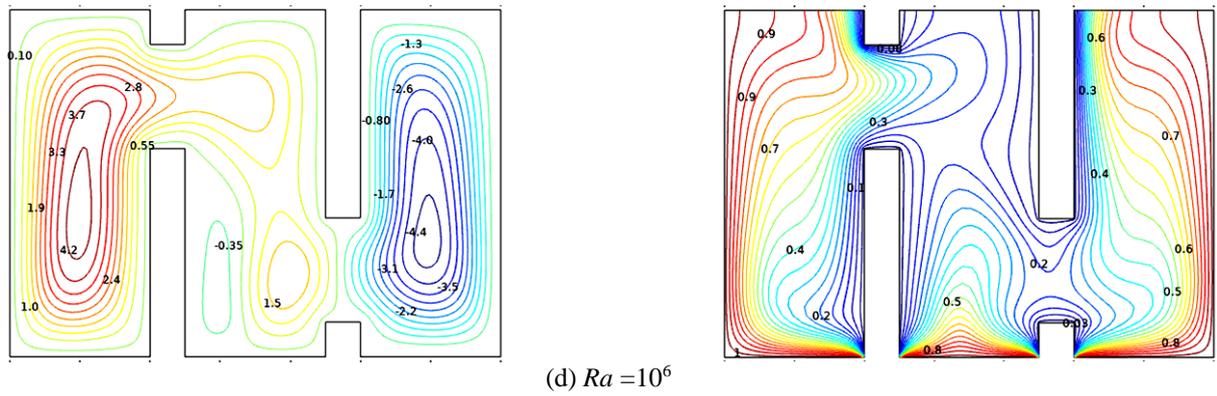
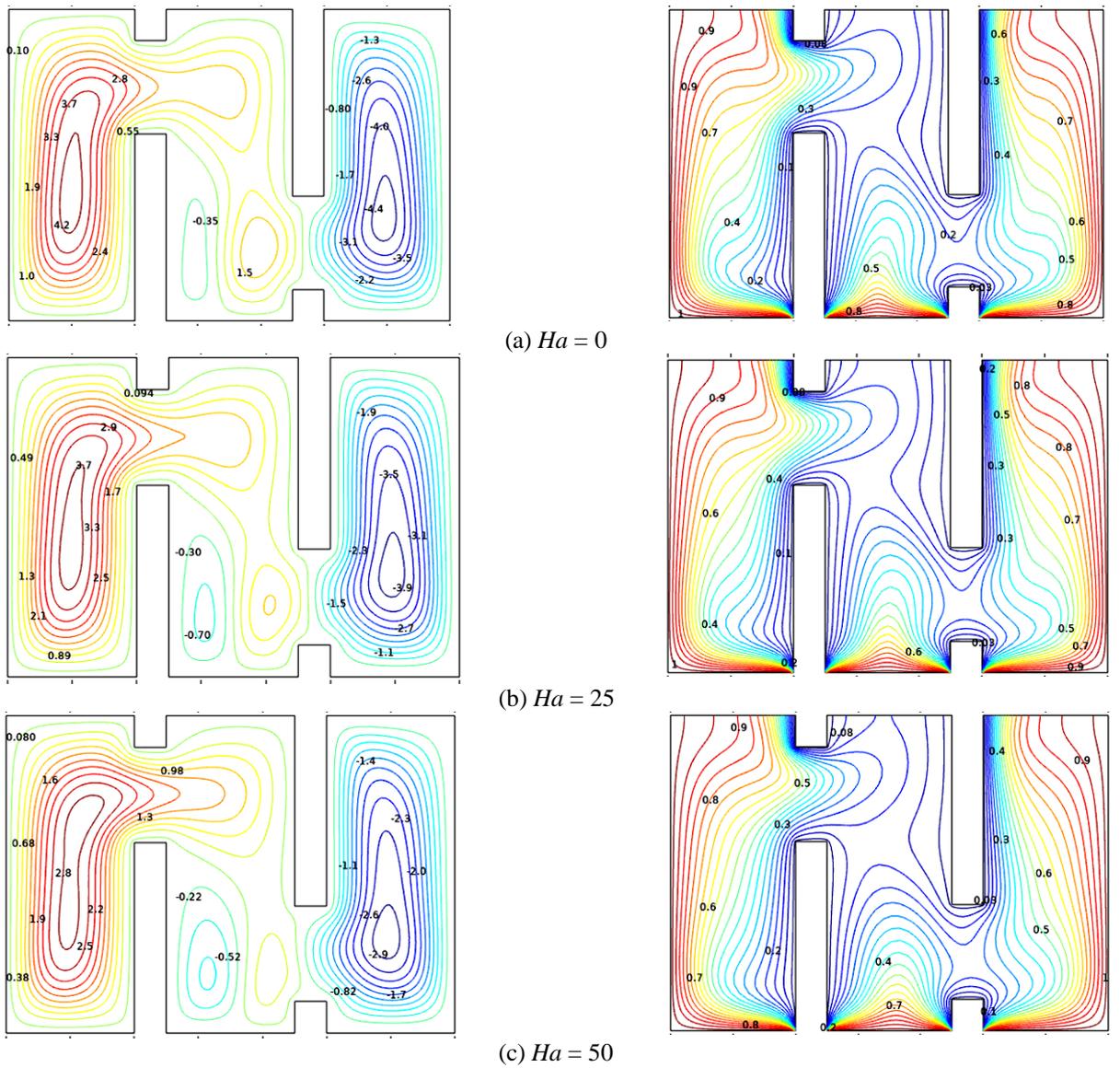


Figure 3. Variations of the streamlines (left) and isotherms (right) with various Rayleigh number ( $Ra$ ),  $Ha = 0$ ,  $Da = 0.1$ ,  $\varepsilon = 0.4$  and  $\varphi = 0.05$ .



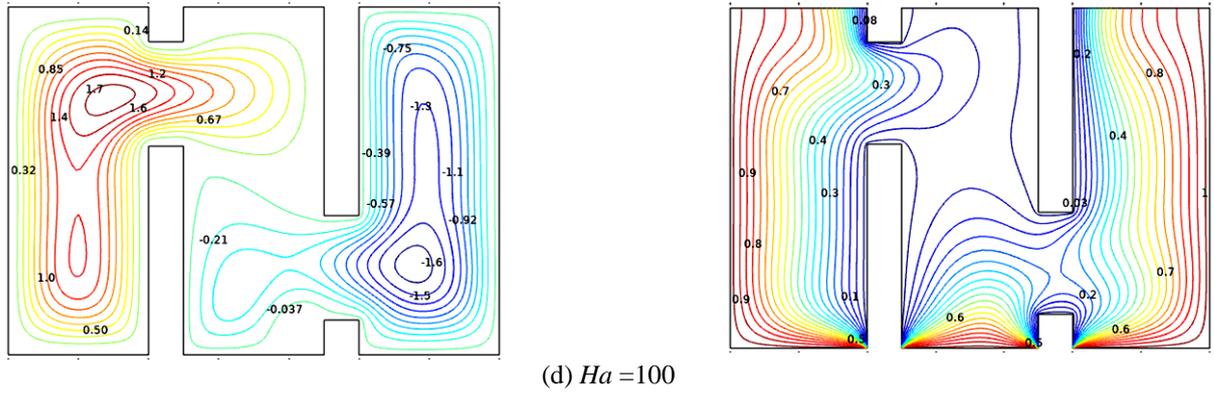


Figure 4. Variations of the streamlines (left) and isotherms (right) with various Hartmann number ( $Ha$ ),  $\varphi = 0.02$ ,  $Ra = 10^6$  and  $Da = 0.1$ .

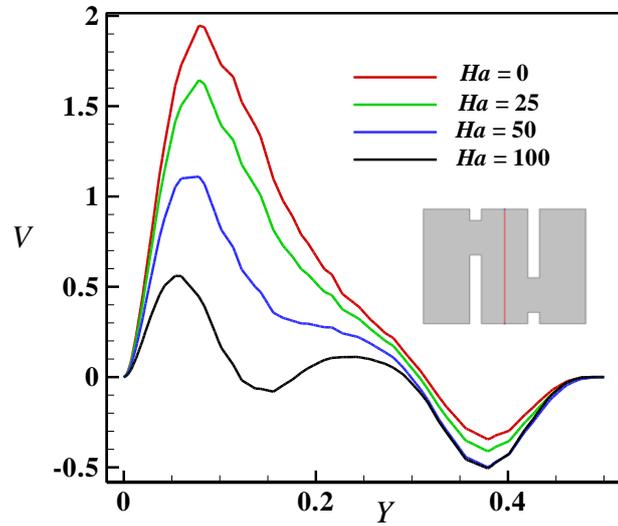


Figure 5. Vertical velocity component ( $V$ ) vs  $Ha$  for  $\varphi = 0.02$ ,  $Ra = 10^5$ .

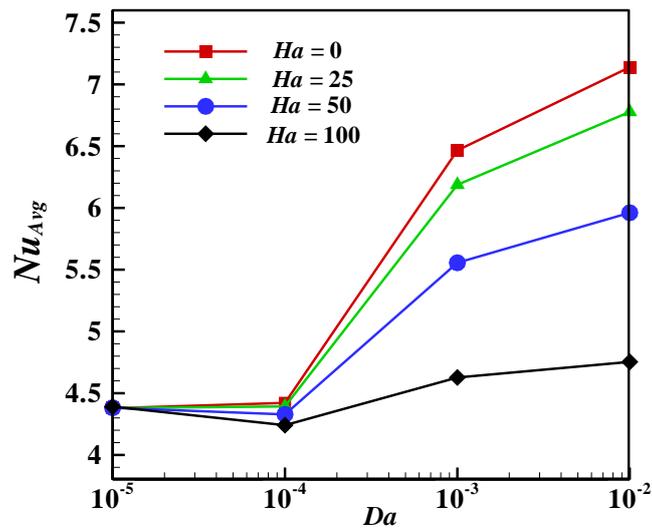


Figure 6.  $Nu_{Avg}$  vs  $Da$  for various  $Ha$ .

Figures 4 and 3 illustrate the effect of the  $Ra$  numbers and  $Ha$  numbers on the streamlines and isotherms, respectively. For various Rayleigh numbers ( $10^2 - 10^6$ ) the study are performed.

For the low numbers of  $Ra$  the lines of the isotherms are vertical straight lines without deformation, this is very well explained by the dominant of the conductive mode. (Figs. 3 a and b)

But with the increase in the value of the  $Ra$  number the lines of the isotherms are deformed favoring the convective mode, and this mode of transfer persists for large values of  $Ra$  where the deformation of the isotherms is clear. (Fig. 3d).

Two large separate towing cells; the negative (on the right) and the positive (on the left) appear in the studied system. Keeping in mind that the maximum and minimum values are located at the center of the cells, we can clearly notice that:

1. this value increases with the increase in the  $Ra$  number where the vortex widens and the convective mode reigns in the flow, of which:  $\Psi_{\max}=0.0069$  for  $Ra = 10^2$  and  $\Psi_{\max}= 4.1$  for  $Ra = 10^6$ . (Fig. 3)

2. this value increases with the rise in the intensity of the magnetic field, of which without magnetic field:  $\Psi_{\min}=-4.4$  and for  $Ha = 100$   $\Psi_{\min}= -1.6$ . (Fig. 4)

In order to study the effect of the application of the magnetic field on this porous enclosure, values of  $Ha$  between 0 and 100 and  $Da$  between  $10^{-2}$  and  $10^{-4}$  are used. Figure 5 shows the vertical velocity profiles ( $V$ ) for a horizontal plane located at the mid-section of the enclosure. Here, the plotted values of the velocity components indicate the direction of the fluid movement within the enclosure. By comparing the velocity profiles in the two figures, it is evident that the amplitude of the velocity components decreases with rising strength of the magnetic field. The substitution in the  $Nu_{\text{avg}}$  is demonstrated by Figure 6 along with the hot wall for various  $Da$  and  $Ha$  values, at  $Ra = 10^5$ ,  $\phi = 0,02$ ,  $\varepsilon = 0.4$ . Similarly, it can be concluded that when the  $Da$  augments, the  $Nu_{\text{avg}}$  enhanced. Accordingly, for the  $Da$  at high values (i.e.,  $Da = 10^{-2}$ ), it is noticed that the process of the heat exchange is sufficient. Regarding the effect of  $Ha$  on heat transfer, it can be predicted that as  $Ha$  increases,  $Nu_{\text{avg}}$  decreases, this is due to the external magnetic field, which dominates at the suppression of the flow field. As results, for a good transfer we must lower the  $Ha$  number.

Regarding the effect of  $Ha$  on the  $Nu_{\text{avg}}$  findings, it can be predicted that as the  $Ha$  increases, they would decrease. This behavior can be attributed to the outside magnetic field, which dominates to the suppression of the flow field. As a consequence, the  $Nu_{\text{avg}}$  is predicted to drop with the  $Ha$ .

## VI. Main results

In this investigation, the effects of magnetic field on natural convection in a special enclosure filled with nanofluid are studied numerically. The dimensionless governing equations are solved using Galerkin finite element method. Computations are performed to analyze the effects of pertinent parameters on the fluid flow, temperature and heat transfer rate, respectively.

The important conclusions can be compiled as:

1. Fluid flow strength accelerates significantly with rising  $Ra$  and decelerates with an augmentation in magnetic field strength. Isotherms distributions become more concentrated with greater  $Ra$  and lower  $Ha$ .
2. The rise in  $Ra$  increases the convective heat transfer coefficient, and the convective mode persists in the range of  $10^5$  to  $10^6$ .
3. The maximum and minimum values of the stream function rise with the increase in the value of the  $Ra$  number and the  $Ha$  number.
4. The magnetic field is a good regulator for the fluid flow and the heat transfer.
5. For good heat transfer, it is necessary to reduce the Hartmann number and increase the  $Da$  number.

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